Practical, simple and cost-effective alternatives for heating liquids in-line or in an open tank



FEATURES

- Simple design with no moving parts to wear out.
- · No packing glands.
- No lubrication required.
- Virtually maintenance-free.
- Easy to install without special structures or foundations.
- Cast or fabricated constructions.
- Variety of materials to suit specific characteristics of the process liquids.
- Critical flow paths machined smoothly with no abrupt turns or steps, producing the most efficient flow during the motive function.

GENERAL APPLICATION

Applications for inline heaters include: circulating cleaning solutions, pasteurization, producing scalding sprays, sterilization, heating water, blanching, exchanging heat, degreasing, heating slurries, laundering, cooking, pickling, bonderizing, quenching and tempering. For open tank heaters: cooking grain, mash or starch, heating and circulating, mixing.

TECHNICAL DATA

Materials: Bronze, carbon steel, 316SS

Sizes: 1/4" to 12"

Pressure (max): 150 psig (10.3 barg)

250 psig (17.2 barg)



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PENBERTHY SERIES ELL, HLM, SRH AND CTE2 FOR HEATING LIQUIDS HEATING LIQUIDS IN LINE

PRODUCT OVERVIEW

Three series of Penberthy steam jet heaters are used for heating liquids in line. One models is available for heating liquids in tanks.

Models ELL, HLM and SRH in-line mixers can heat in-line while transporting the process media. Steam jet heaters optimize the condensation of steam into the motive medium to heat the fluid.

CTE2 circulating tank eductor heaters are open tank heaters that combine steam and liquid in vessels where contents may be recirculated.

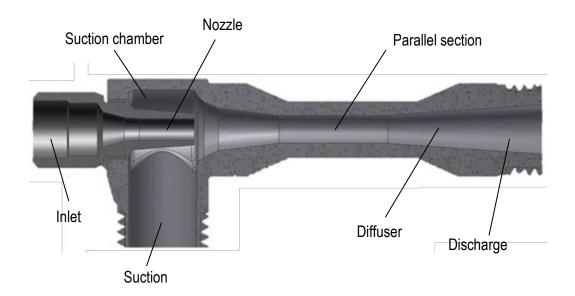
OPERATION

Steam jet heaters optimize the condensing of steam into operating liquids to provide efficient fluid heating. They re essentially jet pumps and, as such, operate on the principle of one fluid entraining a second fluid.

Steam jet heaters have three common features (designations may vary according to design): inlet, suction and discharge.

Inlet – The operating liquid (sometimes called the motive) under pressure enters the inlet and travels through the nozzle into the suction chamber. The nozzle converts the pressure of the operating liquid stream emerging from the inlet nozzle, lowering the pressure in the suction chamber. The resulting action causes the steam in the suction chamber to flow toward the discharge.

Discharge (sometimes called outlet) – The entrained steam in the suction chamber mixes and condenses into the operating liquid and acquires part of its energy, flowing into the parallel section. In the diffuser section, part of the velocity of the mixture is converted into a pressure greater than the suction pressure, but lower than the inlet pressure.





USING LIQUID AS THE OPERATING (inlet) MEDIUM, STEAM AS A SUCTION STREAM HEAT SOURCE

Models ELL, HLM and SRH are available for heating liquids in line. These models are ejector type heaters capable of operating at steam pressures lower than the operating liquid pressure. They offer much higher BTU input than a comparable steam ring heater, while incurring a higher inlet-to-discharge pressure drop.

ELL and HLM models are typically used as single pass devices. The SRH-steam ring heater is a low pressure drop inline heater for single pass or multi-pass applications.

These inline heaters provide heat and operating pressure for cleaning solution circulation, producing scalding sprays, heating water and slurries, exchanging heat and cooking. The table lists the operating parameters of each.

TABLE 1 - MODEL SPECIFICATIONS

Model	ELL Low steam pressure	HLM High steam pressure	SRH Steam ring heater			
Steam pressure	up to 45 psig (310 kPag)	up to 120 psig** (830 kPag)	up to 150 psig (1035 kPag)			
Max. water temp. rise (ΔT)*	up to 182°F (83°C)	up to 216°F (102°C)	up to 200°F (93°C)			
Max. capacity	5000 gpm (18925 lpm)	5000 gpm (18925 lpm)	500 gpm (1893 lpm)			

^{*} Based on 60°F inlet water

SELECTING THE APPROPRIATE HEATER

To choose the appropriate inline heater for the application, compare the available steam pressure to the line pressure of the liquid to be heated. If the steam pressure is lower than or equal to the liquid pressure, an ELL or HLM heater must be used. If the steam pressure is higher than the liquid pressure, the ELL, HLM or SRH can be used. In this latter case, the ELL and HLM offer higher steam flows than the SRH (see Table 1). In on/off heating applications or during periods when steam input is halted, the ELL and HLM produce very large pressure drops. The SRH maintains its low pressure drop characteristics even when steam input is removed.

When using the HLM or ELL heater and when the discharge pressure exceeds one third of the operating pressure, the heater discharge pressure should be lowered during start-up, until the heater is operating, i.e. until both steam and water flows are established.



^{**} Max. steam pressure for iron body material, 60 psig

HEATING LIQUIDS IN LINE

ELL. HLM MODELS

Each of the two models is available in 15 sizes from $\frac{1}{2}$ " to 12" suction and discharge. Units are cast construction in $\frac{1}{2}$ " through 4" sizes. Sizes 4" through 12" are available in fabricated construction.

Cast unit connections

Units ½" through 3" in size have NPT inlet, suction and discharge connections. 4" size has NPT inlet and flanged suction and discharge. Flanges on cast units are raised faced with holes, sizes and spacing corresponding to 150 lb ASME flanges.

Fabricated unit connections

All fabricated ELL and HLM units, 4" through 12" sizes, have raised faced flanges with holes, sizes and spacing corresponding to 150 lb ASME flanges.

NOTE

Always specify material, model and unit size when ordering.

TABLE 2 - MODEL CONSTRUCTION DATA

Model	ELL, HLM	Standard materials
Sizes available	½"A - 4"	Cast: bronze, C. steel, 316 STS
	4" and up	Fabricated: Carbon steel, 316 STS

The ELL and HLM heaters operate with direct connections from steam and liquid lines. Though application and performance characteristics vary between the two, steam consumption is equal for a given temperature rise. As a general rule, steam flow is calculated as follows:

$$Q_s = \frac{Q_m \Delta T}{120}$$

Where:

Qs = steam flow in lbs/min

Qm = operating liquid in gpm

 ΔT = temperature rise in °F

The following general operating characteristics will help in selecting the correct model heater:

ELL operates generally low to medium suction steam pressure (from 25" Hg vacuum to 45 psig). Performance capabilities include up to 182 °F temperature rise and up to 94 psig discharge pressure.

HLM operates over the widest range of performance characteristics and is usually the choice for most heating applications. It operates in a high steam pressure range (up to 120 psig), produces a high temperature rise (up to 216 °F) at a high discharge pressure (up to 184 psig).

Heater selection using performance charts

The following information is required to select the correct model:

- Operating liquid (for liquids other than water, consult the factory)
- Operating liquid inlet pressure, psig (h_m)
- Desired operating liquid capacity, gpm (Q_m)
- Operating liquid inlet temperature, °F (contact the factory when operating liquid inlet temperature exceeds 100°F)
- Desired temperature rise, °F (ΔT)
- Available steam pressure, psig (h_s)
- Minimum discharge pressure required, psig (h_d)
- Quality of steam available, i.e. saturated or superheated



HEATING LIQUIDS IN LINE

ELL. HLM MODELS

Evaluating both the ELL and HLM is recommended before choosing the model that best fits the operating conditions, by using the following procedure:

- Step 1 Refer to the heater performance chart for the selected model.

 Locate the operating liquid (water) pressure psig (h_m) for your application.
- Step 2 In this (h_m) row, read across to find the desired temp. rise °F and note the steam pressure (h_s), disch. press. psig (h_s) and liquid flow (Q_m).

Step 3 – The performance charts indicate the capacities of 1 $\frac{1}{2}$ " units. To select units closest to actual requirements (one that equals or exceeds the required low) it may be necessary to calculate several sizes other than 1 $\frac{1}{2}$ " (refer to the example).

Example

To heat operating liquid 100 gpm water (Q_m) from 60 to 185° (ΔT 125°F)

Operating liquid, psig (h_m): 40
Available steam pressure (h_s): 150
Minimum discharge pressure required (h_d): 25

From the HLM performance chart:

Opposite 40 psig operating liquid inlet pressure (h_m) locate desired temperature rise (ΔT) 125 °F (between 121 and 132). The required steam pressure (h_s) will be between 40 and 45 psig. The discharge pressure (h_d) is greater than the minimum pressure required. The liquid flow (Q_m) is 23 gpm which is below the requirement of 100 gpm.

To select a larger unit for the 100 gpm requirement, try the next available sizes – the 2", 2 $\frac{1}{2}$ ", and 3" units using the capacity factors in the chart.

2" size CF = 1.82
Heating capacity = 23*1.82 = 41 gpm (too low)
2 ½" size CF = 3.17
Heating capacity = 23*3.17 = 73 gpm (too low)
3" size CF = 5.92
Heating capacity = 23*5.92 = 136 gpm (exceeds requirements)

Repeat this procedure for the ELL

In this example, the ELL-3 comes closest to fitting the requirements. However, the steam pressure supplied to the ELL-3 would have to be throttled down from 150 psig to only 8 psig. This degree of throttling may be impractical, so the HLM-3 would be the more appropriate choice.



ELL, HLM MODELS - PERFORMANCE

TABLE 3 - 11/2 MODEL ELL HEATER PERFORMANCE CHART (water)

Operating													Stear	-														
water, psig	Data	li	nches	Hg. va	acuum	1								- 1	oun	ds pe	r squ	ıare İ	inch g	jauge	•							
(hm)	description	25"	20"	15"	10"	5"	0	2	4	5	6	8	10	12	14	15	16	18	20	22	24	25	26	28	30	35	40	45
20	•	-	-	40	60	77	100	115	126	133	140	150	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	••	-	-	0	0	8	10	12	14	14	14	14	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	***	-	-	10	10	10	15	15	15	14	14	14	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-
30	•	9	24	36	56	69	86	100	113	118	123	136	144	154	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	••	0	5	8	15	18	19	20	21	21	21	21	21	21	-	-	-	-	-	-	-	-	-	-	-	-	-	-
	***	21	21	21	21	20	20	19	18	18	18	17	17	15	-	-	-	-	-	-	-	-	-	-	-	-	-	-
40	•	- 11	25	36	52	85	80	90	99	105	111	128	132	143	153	-	-	-	-	-	-	-	-	-	-	-	-	-
	••	5	6	13	18	22	25	26	27	28	29	29	30	30	30	-	-	-	-	-	-	-	-	-	-	-	-	-
	***	23	23	23	23	22	22	22	22	21	21	20	20	19	19	-	-	-	-	-	-	-	-	-	-	-	-	-
50	•	14	22	36	48	60	79	83	92	96	100	111	122	130	139	145	150	-	-	-	-	-	-	-	-	-	-	-
	••	8	10	11	19	24	27	30	31	32	34	35	36	36	37	37	37	-	-	-	-	-	-	-	-	-	-	-
	***	25	25	25	25	25	25	24	24	24	23	23	22	22	22	21	21	-	-	-	-	-	-	-	-	-	-	-
60	•	14	22	31	43	57	71	76	84	89	94	104	112	120	126	131	134	147	-	-	-	-	-	-	-	-	-	-
	••	12	14	16	24	28	29	32	33	34	36	39	41	42	43	43	41	41	-	-	-	-	-	-	-	-	-	-
	***	27	27	27	27	27	27	26	26	26	26	25	25	24	24	24	23	23	-	-	-	-	-	-	-	-	-	-
70	•	14	34	36	47	56	64	73	78	83	88	96	105	112	122	125	128	140	148	-	-	-	-	-	-	-	-	-
	••	13.5	16	18	28	30	35	38	38	38	39	42	44	44	44	44	44	44	44	-	-	-	-	-	-	-	-	-
	***	29	29	29	29	29	29	29	20	20	20	27	27	27	27	26	26	26	26	-	-	-	-	-	-	-	-	-
80	•	10	20	32	44	54	82	88	78	80	82	90	97	104	112	115	118	127	144	150	-	-	-	-	-	-	-	-
	••	17	18	21	26	32	37	38	40	42	44	45	46	49	48	48	48	48	48	48	-	-	-	-	-	-	-	-
	***	31	31	31	31	31	31	31	31	31	30	30	29	29	29	28	28	28	28	28	-	-	-	-	-	-	-	-
90	•	10	22	30	42	50	64	65	72	76	80	88	92	100	108	111	113	120	128	138	141	-	-	-	-	-	-	-
	••	20	22	23	27	35	39	42	44	45	48	58	52	53	56	56	57	59	59	59	59	-	-	-	-	-	-	-
	***	32	32	32	32	32	32	32	32	32	32	32	32	31	31	31	31	30	30	29	29	-	-	-	-	-	-	-
100	•	7	17	26	40	48	68	70	72	74	80	86	92	95	99	102	108	114	120	127	134	140	144	149	154	172	182	-
	••	23	24	26	29	35	42	44	46	48	51	54	56	57	58	59	60	63	65	67	69	70	71	72	73	76	76	-
	***	33	33	33	33	33	33	33	32	32	32	32	32	32	32	32	31	31	31	31	30	30	30	30	30	30	30	-
120	•	7	10	20	37	44	59	63	67	69	73	76	82	88	92	97	101	106	111	116	121	125	127	132	137	155	169	180
	••	28	30	32	34	37	48	51	53	54	56	59	61	64	67	68	69	71	73	76	78	80	81	82	83	86	90	90
	•••	36	36	36	36	36	36	36	36	36	36	36	35	35	35	35	35	34	34	34	33	33	33	32	32	32	32	32
140	•	6	14	24	34	43	54	58	61	63	67	74	80	84	88	91	94	98	104	108	112	114	118	124	130	140	156	168
	••	34	38	38	41	43	50	54	58	60	62	68	69	72	74	75	76	78	80	83	85	88	88	91	94	94	94	94
	***	39	39	39	39	39	39	39	39	39	39	38	38	38	38	38	38	38	38	37	37	37	37	37	37	37	37	37

^{*} Temp rise - °F (ΔT)

NOTE

All data based on 32°-100°F operating liquid temperatures. For other temperatures, consult factory.

CAUTION

Attempted operation within the areas to the right of the figures will cause uncondensed steam to discharge from the heater.



^{**} Disch press - psig (h_d)

^{***} Liquid flow - gpm (Qm)

ELL, HLM MODELS - PERFORMANCE

TABLE 4 - 11/2 MODEL HLM HEATER PERFORMANCE CHART (water)

Operating											Stea	m pre	ssure	(h _s)									
water, psig	Data		Inches	s Hg. Va	acuum								Pound	ls per	squar	inch	gauge						
(hm)	description	25"	20"	15"	10"	5"	5	10	15	20	25	30	35	40	45	50	60	70	80	90	100	110	120
10	•	-	-	24	32	40	55	64	106	127	144	166	-	-	-	-	-	-	-	-	-	-	-
	••	-	-	4	4	6	17	20	24.5	30.5	34	30	-	-	-	-	-	-	-	-	-	-	-
	***	-	-	17	17	16	16	15	15	14	14	12	-	-	-	-	-	-	-	-	-	-	-
20	•	-	15	20	25	34	61	64	80	88	107	120	134	152	-	-	-	-	-	-	-	-	-
	••	-	4	7	10	15	20	25	30	35	30	42	46	51	-	-	-	-	-	-	-	-	-
	•••	-	20	20	20	20	20	19	19	18	18	18	17	16	-	-	-	-	-	-	-	-	-
30	•	1	12	18	23	30	55	58	65	77	90	103	114	128	140	153	185	-	-	-	-	-	-
	**	5	7	8.5	11	15	22	27	33	37	41	45	52	55	60	65	75	-	-	-	-	-	-
	***	23	23	23	23	22	23	23	22	22	22	22	22	20	20	19	18	-	-	-	-	-	-
40	•	4	10	14	20	27	42	54	57	67	81	91	102	121	132	144	170	190	-	-	-	-	-
	••	8	11	14	17	20	25	28	32	37	42	48	53	57	62	68	77	80	-	-	-	-	-
		25	25	25	25	25	25	25	25	24	24	24	23	23	23	22	21	21	-	-	-	-	-
50		3	6	14	19	22	36	47	57	68	80	90	102	112	122	132	161	180	200	-	-	-	-
	•••	12	15	17	21 28	23.5 28	30	35 27	40 27	45	50 26	55 26	64 26	68 25	70 25	75 24	85 23	96 23	101 22	-	-	-	-
60	•	28	28	28 12	18	28	27 34	44	54	26 64	73	82	92	100	110	120	142	162	184	204	-	-	-
au		14	19	21	24	27	35	36	44	50	55	61	66	71	75	80	83	101	104	105	-	-	-
	•••	30	30	30	30	30	30	30	29	29	29	28	28	28	27	27	25	25	24	24	-		
70		3	7	12	17	21	33	42	51	60	69	78	85	94	103	112	130	148	168	188	200		
70	••	18	21	25	28	31	38	43	48	53	58	65	69	73	79	85	92	104	103	122	133	_	_
	•••	32	32	32	32	32	32	32	31	31	31	31	30	30	30	30	29	28	27	26	26	_	_
80	•	4	8	12	15	20	32	40	46	55	64	71	80	90	95	105	115	142	154	165	174	212	_
	••	22	26	29.5	31	34	42	48	52	57	62	65	72	72	79	86	91	107	113	128	138	142	_
	***	33	33	33	33	33	33	33	33	33	32	32	32	32	31	31	31	30	30	29	28	27	_
90	•	3	8	11	15	20	30	37	44	51	60	69	76	86	91	97	116	132	146	160	175	196	215
	••	27	29	33	36	38	43	51	55	61	66	72	76	81	85	90	101	112	120	131	140	144	163
	***	35	35	35	35	35	35	35	35	34	34	34	34	34	34	33	33	32	32	31	31	29	29
100	•	2	6	10	14	19	30	38	41	50	56	62	70	80	87	94	108	123	140	150	164	184	196
	••	28	30	32.5	38	41	45	54	59	64	69	73	78	84	89	95	104	114	126	132	142	154	155
	***	36	36	36	36	36	36	36	36	36	36	36	36	36	35	35	34	34	33	33	33	32	31
120	•	2	6	10	13	17	28	30	39	45	52	59	65	72	79	88	98	115	128	145	155	168	189
	**	30	37	40	45	49	58	61	66	71	78	80	88	91	96	100	112	123	132	145	150	161	174
	***	40	40	40	40	40	40	40	40	40	40	39	39	39	39	39	38	37	37	36	36	35	35
140	•	2	5	10	12	15	27	30	36	44	49	55	61	66	71	77	90	103	116	125	144	158	170
	**	38	47	50	53	58	64	67	72	82	83	88	96	97	102	108	120	130	139	148	162	172	184
	•••	43	43	43	43	43	43	43	42	42	42	42	42	42	42	42	42	40	40	40	40	39	39

^{*} Temp rise - °F (ΔT)

NOTE

All data based on 32°-100°F operating liquid temperatures. For other temperatures, consult factory.

CAUTION

Attempted operation within the areas to the right of the figures will cause uncondensed steam to discharge from the heater.

TABLE 5 - ELL, HLM CAPACITY FACTOR

1/2A	1/2B	1/2	3/4	1	11/4	11/2	2	21/2	3	4	6	8	10	12
0.03	0.047	0.121	0.208	0.344	0.613	1	1.82	3.17	5.92	11.8	24	49	71	123



^{**} Disch press - psig (hd)

^{***} Liquid flow - gpm (Qm)

ELL, HLM MODELS - PERFORMANCE

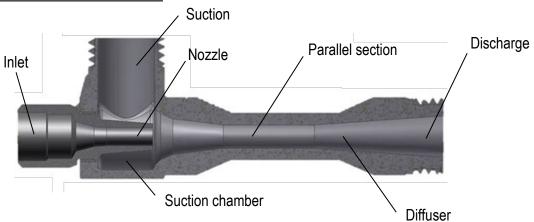


TABLE 6 - CAST ELL. HLM DIMENSIONS (in inches)

IABLE 6 - CAS	I ELL, HLM DIME	11310143 (111 11	iciies)			
Size	A	В	С	D	E*	F*
1/2 A	43/8	11/2	11/4	1/4	1/2	1/2
1/2 B	43/8	11/2	11/4	1/4	1/2	1/2
1/2	41/2	15/8	11/4	3/8	1/2	1/2
3/4	51/8	2	11/2	1/2	3/4	3/4
1	71/8	21/4	13/4	3/4	1	1
11/4	9	21/2	21/4	1	11/4	11/4
11/2	11	23/4	21/2	1	11/2	11/2
2	143/8	31/8	3	11/4	2	2
21/2	181/2	31/2	41/8	11/2	21/2	21/2
3	231/8	4	5	2	3	3
4	327/6	5	6	3	/+**	/+**

^{*} All cast units have NPT connections except: 4" size has NPT inlet, flanged suction and discharge

flange

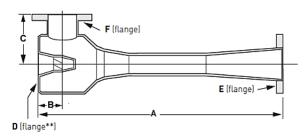
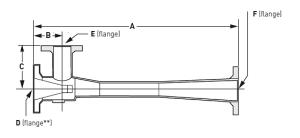


TABLE 7 - FABRICATED ELL DIMENSIONS (in inches)

IADLE / - FADI	KICA I ED ELL DIM	ENSIONS (III	iliciies)			
Size	Α	В	С	D**	E	F
4	381/4	51/4	8	3	4	4
6	521/8	51/8	91/2	4	6	6
8	747/16	87/16	13	6	8	8
10	873/8	10¾	14	8	10	10
12	1103/4	113/4	18	10	12	12

^{**} Inlet flanges on fabricated units have blind tapped holes.



FABLE 8 - FAB	ABLE 8 - FABRICATED HLM DIMENSIONS (in inches)												
Size	Α	В	С	D	E	F							
4	381/4	51/4	8	4	3	4							
6	521/8	57/s	91/2	6	4	6							
8	747/16	87/16	13	8	6	8							
10	87%	10%	14	10	8	10							
12	110¾	113/4	18	12	10	12							



MODEL SRH

SRH (Steam Ring Heaters) are compact, inline units with low pressure drop. SRH units inject steam through a ring-shaped opening within an enlargement in the pipeline. Liquid passes through and around the ring. Heat is introduced by the direct condensation of steam. They provide fast temperature correction noiselessly and without vibration if applied correctly. Because the liquid flow area is unrestricted, pressure drops across the heater are minimized. This will reduce the horsepower requirements for the operating liquid pump.

Model SRH is available in inlet and outlet sizes of 1 ½", 2" and 3" threaded and 6" flanged.

NOTE

Always specify material, model and unit size when ordering.

TABLE 9 - MODEL CONSTRUCTION DATA

Model	SRH	Standard materials
Sizes available	11/2", 2", 3", 6"	Bronze, carbon steel, 316 STS

The following information is required to select the correct model:

Operating liquid (for liquids other than water, consult the factory)

- Operating liquid inlet pressure, psig (h_m)
- Desired operating liquid capacity, gpm (Q_m)
- Operating liquid inlet temperature, °F (contact the factory when operating liquid inlet temperature exceeds 100°F)
- Desired temperature rise, °F (∆T)
- Available steam pressure, psig (h_s)
- Minimum discharge pressure required, psig (h_d)
- Quality of steam available (i.e. saturated or superheated)
- Maximum pressure drop (ΔP). Refer to Tables 11, 12 and 13

DIMENSIONS

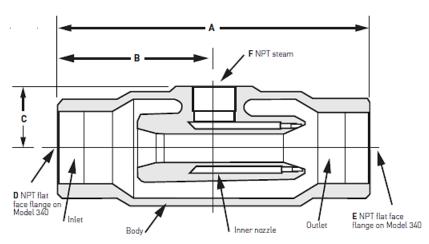


TABLE 10 - SRH DIMENSIONS (in inches)

Unit	Inlet	Outlet	Steam	Α	В	C
310	11/2	11/2	1	6%	3%	13/4
320	2	2	11/4	93/4	47/a	17/a
330	3	3	17/a	10¾	53/8	21/2
340	6(*)	6[*]	2	10	5	3¾

Flanged.



HEATING LIQUIDS IN LINE

MODEL SRH

The following steps are provided for selecting the correct size SRH:

- Step 1 In the steam consumption chart (Table 13) locate the point where the desired water flow gpm and temperature rise in °F (ΔT) intersect. Read off the steam consumption in lbs/min.
- Step 2 In the SRH performance chart (Table 12), locate the point where the operating water press. psig (h_m) and steam pressures (h_s) intersect. These represent the various steam consumptions for individual SRH units. Those with consumptions from the chart in Step 1 indicate the SRH model to choose
- Step 3 If the steam flow shown for the model selected is greater than required, throttle the steam to a pressure that will provide the required steam flow.

To determine the pressure drop for the selected unit use the formula as shown.

The rational flow formula is: $dp = \left(\frac{GPM}{C_V}\right)^2 G$ or $GPM = C_V \frac{dp}{dp} G$

GPM - U.S. gallons per minute

Cv - Unit flow coefficient

G - Specific gravity

dp - Pressure drop across the unit, psid

Cv is defined as the number of U.S. gallons of water per minute that will flow through the unit at a

1 psi pressure drop.

Example:

To find the pressure drop for a 320 heater with a flow of 150 gpm:

$$dp = \left[\frac{GPM}{C_V}\right]^2 G$$

$$dp = \left[\frac{150}{75}\right]^2 [1]$$

dp = 4 psid

Example

To heat 150 gpm water from 70 to 85 °F (Δ T 15 °F) Operating liquid inlet pressure, psig (h_m): 40 Available steam pressure, psig (h_s): 80 Maximum pressure drop, psig (Δ P): 5

From Step 1 of the procedure, the steam consumption is 18.7 lb/min.

From Step 2 note the steam consumption closest to 18.7. Model 310 will handle 18 lb/min, just below our requirement and model 320 will handle 27 lb/min.

From Step 3, select the model with the higher available steam consumption and throttle the steam accordingly. The performance chart (Table 12) indicates that the model 320 should be throttled to slightly above 60 psig to achieve the desired consumption of 18.7 lbs/min.

Note that the maximum allowable pressure drop (Δ P) is 5 psig in this example. Using the rational flow formula example for the model 320 selected, we see the pressure drop is 4 psig below the stated maximum.



MODEL SRH - PERFORMANCE

TABLE 11 - SRH SIZING COEFFICIENT

Unit	C _v liquid sizing coefficient (gpm)	Heat input max. (BTU Min. at 150 psig wsp)*
310	50	32000
320	75	48000
330	125	79000
340	350	128000

^{*} Working steam pressure (at operating liquid pressure of 80 psig)

TABLE 12 - SRH PERFORMANCE - STEAM CONSUMPTION IN lbs/min (Qs)

Op. water press.**,						Ste	eam press	ure, psig (h _s)				
psig (h _m)	Model	20	30	40	50	60	70	80	90	100	120	140	150
10	310	6	9	11	13	15	17	19	21	23	26	30	32
	320	9	14	17	20	22	25	28	31	34	40	45	48
	330	16	23	28	33	37	42	47	52	56	66	75	79
	340	25	36	45	52	60	68	75	83	90	106	121	128
20	310	-	7	10	13	15	17	18	21	23	26	30	32
	320	-	10	15	19	22	25	28	31	34	40	45	47
	330	-	17	25	31	37	42	47	52	56	66	75	79
	340	-	28	40	50	59	68	75	83	90	106	121	127
40	310	-	-	-	9	12	15	18	20	23	26	30	32
	320	-	-	-	13	18	23	27	31	34	40	45	47
	330	-	-	-	22	31	38	45	51	56	66	75	79
	340	-	-	-	35	49	61	72	82	90	106	121	127
60	310	-	-	-	-	-	11	15	19	21	26	30	32
	320	-	-	-	-	-	16	22	28	32	39	45	47
	330	-	-	-	-	-	26	37	46	53	65	75	79
	340	-	-	-	-	-	42	60	74	86	104	120	126
80	310	-	-	-	-	-	-	-	13	18	25	30	32
	320	-	-	-	-	-	-	-	20	27	37	44	47
	330	-	-	-	-	-	-	-	32	44	61	74	78
	340	-	-	-	-	-	-	-	52	71	98	119	126

All data based on 32° to 100°F inlet water temperature (Tm). For other inlet water temperatures consult the factory.

NOTE

Operation shown in bold is susceptible to high frequency noise.



^{**(}with water flowing)

MODEL SRH - PERFORMANCE

TABLE 13 - SRH STEAM CONSUMPTION (lbs per minute) RELATED TO TEMPERATURE RISE AND WATER FLOW*

	Temperature rise in °F (ΔT)														
Water flow, gpm (Q _m)	5	10	15	20	25	30	35	40	45	50	55	60	65	70	75
10	0.4	8.0	1.2	1.7	2.1	2.5	2.9	3.3	3.7	4.2	4.6	5.0	5.4	5.8	6.2
15	0.6	1.2	1.9	2.5	3.1	3.7	4.4	5.0	5.6	6.2	6.9	7.5	8.1	8.7	9.4
20	8.0	1.7	2.5	3.3	4.2	5.0	5.8	6.7	7.5	8.3	9.2	10.0	10.8	11.7	12.5
25	1.0	2.1	3.1	4.2	5.2	6.2	7.3	8.3	9.4	10.4	11.4	12.5	13.5	14.5	15.7
35	1.6	2.9	4.4	5.8	7.3	8.7	10.2	11.7	13.1	14.6	16.0	17.6	18.8	20.0	22.0
45	1.9	3.7	5.2	7.5	9.4	11.2	13.1	15.0	16.9	18.7	21.0	22.0	24.0	28.0	28.0
50	2.5	5.0	7.5	10.3	12.5	15.0	17.5	20.0	22.0	25.0	27.0	30.0	32.0	35.0	37.0
60	3.3	6.7	10.0	13.3	16.7	20.0	23.0	27.0	30.0	33.0	37.0	40.0	43.0	47.0	50.0
100	4.2	8.3	12.5	16.7	21.0	25.0	29.0	33.0	37.0	42.0	46.0	50.0	54.0	58.0	62.0
125	5.2	10.4	15.8	21.0	27.0	31.0	38.0	42.0	47.0	52.0	57.0	62.0	68.0	73.0	78.0
150	6.2	12.5	18.7	25.0	31.0	37.0	44.0	50.0	55.0	62.0	69.0	75.0	81.0	87.0	94.0
175	7.3	14.6	22.0	29.0	36.0	44.0	51.0	58.0	66.0	73.0	80.0	87.0	95.0	102.0	109.0
200	8.3	16.7	25.0	33.0	42.0	50.0	58.0	67.0	75.0	83.0	92.0	100.0	108.0	117.0	125.0
250	10.4	21.0	31.0	42.0	52.0	62.0	73.0	83.0	94.0	100.0	114.0	125.0	135.0	148.0	158.0
300	12.5	25.0	39.4	50.0	62.0	74.0	85.0	100.0	112.0	124.0	136.0	150.0	162.0	175.0	187.0
400	17.0	33.0	50.0	67.0	83.0	100.0	117.0	133.0	150.0	167.0	183.0	200.0	217.0	233.0	250.0
500	21.0	42.0	62.0	83.0	104.0	125.0	146.0	166.0	187.0	200.0	229.0	250.0	271.0	291.0	312.0

TABLE 13 - SRH STEAM CONSUMPTION (lbs per minute) RELATED TO TEMPERATURE RISE AND WATER FLOW* (continued)

TABLE 10 - SKITSTEAL	. 00.1501		ttoo per	minute)	ILLEA II	-D .O IL	THE LIVE	TORE IN	JE AITD	HAILI		(COIICIIIa	· · · ·		
	Temperature rise in °F (ΔT)														
Water flow, gpm (Q _m)	80	85	90	95	100	110	120	130	140	150	160	170	180	190	200
10	6.7	7.1	7.5	7.9	8.3	9.2	10	10.8	11.7	12.5	13.3	14.2	15	15.8	16.7
15	10.0	10.6	11.2	11.9	12.5	13.7	15	16.2	17.5	18.7	20.0	21.0	22	24.0	25.0
20	13.3	14.2	15.0	15.8	16.7	18.3	20	22.0	23.0	25.0	27.0	28.0	30	32.0	33.0
25	15.7	17.7	18.7	19.8	21.0	23.0	25	27.0	29.0	31.0	33.0	35.0	37	40.0	42.0
35	23.0	25.0	26.0	28.0	29.0	32.0	36	38.0	41.0	44.0	47.0	50.0	52	55.0	58.0
45	30.0	32.0	34.0	36.0	37.0	41.0	45	49.0	52.0	58.0	60.0	64.0	67	71.0	75.0
50	40.0	42.0	45.0	47.0	50.0	55.0	60	65.0	70.0	75.0	80.0	85.0	90	95.0	100.0
60	53.0	57.0	60.0	63.0	67.0	73.0	80	87.0	93.0	100.0	107.0	113.0	120	127.0	133.0
100	67.0	71.0	75.0	79.0	83.0	92.0	100	108.0	117.0	125.0	133.0	142.0	150	158.0	167.0
125	83.0	88.0	94.0	99.0	104.0	115.0	125	135.0	148.0	158.0	167.0	177.0	187	198.0	208.0
150	100.0	105.0	112.0	119.0	125.0	137.0	150	162.0	175.0	187.0	200.0	212.0	225	237.0	250.0
175	117.0	124.0	131.0	136.0	146.0	160.0	175	189.0	204.0	219.0	233.0	243.0	262	277.0	291.0
200	133.0	142.0	150.0	158.0	167.0	183.0	200	217.0	233.0	250.0	267.0	283.0	300	317.0	333.0
250	167.0	177.0	187.0	198.0	208.0	229.0	250	271.0	291.0	312.0	333.0	354.0	375	396.0	416.0
300	200.0	212.0	225.0	237.0	250.0	275.0	300	325.0	350.0	375.0	400.0	425.0	450	475.0	500.0
400	267.0	283.0	300.0	317.0	333.0	367.0	400	433.0	466.0	500.0	533.0	566.0	600	633.0	666.0
500	333.0	354.0	375.0	396.0	416.0	458.0	500	541.0	583.0	625.0	666.0	708.0	750	791.0	833.0

^{*} Based on 60°F inlet water



HEATING LIQUIDS IN LINE

CTE2 circulating tank eductor heaters are open tank heaters that combine steam and liquid in vessels where contents may be recirculated.

Open tank heaters provide circulation and efficient steam-liquid contact superior to coil heating without the noise of direct application. They are installed submerged in the tank.

Using up to 140 psig steam, Penberthy open tank heaters produce maximum temperature rises up to 120°F, depending on the size of the unit.

NOTE

Because of the nature of open tank installations, do not attempt to heat beyond the maximum stated temperature.

The submerged open tank heaters combine steam and liquid or slurry to recirculate the contents of a tank. They are especially suited for cooking, heating and circulating liquids.

Model CTE2 is a versatile heater that can also produce a strong mixing action throughout the tank contents. The CTE2 requires a minimum of 10 psig steam pressure.

TABLE 14 - MODEL SPECIFICATIONS

TABLE 14 THOREE OF EON TOWNS	
Model	CTE - Circulating Tank Eductor
Motive steam pressure	up to 140 psig (966 kPag)
Max. water temp. rise (ΔT)	up to 120°F (49° C)
Max. final tank temp.	up to 160°F (71° C)



HEATING LIQUIDS IN LINE

MODELS CTE2

Model CTE2

The CTE2 (Circulating Tank Eductor) is an ejector-type jet, requiring no nipple, recommended for tanks in multiple installations near and parallel to the tank bottom. Steam inlet sizes range from 3/8" to 3".

TABLE 15 - MODEL CONSTRUCTION DATA

Model	CTE	Standard materials
Sizes	3/8"-4"	Cast: bronze, carbon steel, 316 STS
available	4" and up	Fabricated: Carbon steel, 316 STS

Unit selections using performance charts

The following information is required to select and size tank heaters:

- Tank liquid (if other than water, consult factory)
- Available steam pressure, psig (h_m)
- Desired temperature rise, °F (ΔT)
- Tank capacity, gallons
- Heating time, minutes
- Initial temperature of liquid °F (T_s)

NOTE

Always specify material, model and unit size when ordering.



HEATING LIQUIDS IN LINE

MODEL CTE2

There are two methods provided her for selecting the correct unit.

Method 1 uses the steam consumption table (lb/min of steam).

Method 2 uses the performance table (heating capacity in ghpm-gallons heated per minute).

Method 1

- Step 1 Multiply the total batch gallons by 8.33 lbs to find the weight (if water).
- Step 2 Multiply the result by the number of degrees temperature rise desired and divide this number by 1000 to determine the weight of steam (lbs) to do the job.
- Step 3 Divide this figure by the heating time required (in min.). This figure represents the rate of steam flow in pounds per minute.
- Step 4 Under available steam pressure, locate steam consumption equal to or greater than the requirement. At this point, move to the left and determine the unit size.

Method 1 example

This method can be used in the CTE2 heaters for water.

Operating conditions

Available steam pressure psig (h_m): 40 Desired temperature rise °F (Δ T): 40 Tank capacity, gallons: 800 Heating time, minutes: 60 Initial temperature of liquid °F(T_s): 40

Step 1 - 800 (gallons) x 8.33 (lbs) = 6670 lbs, the weight of water

Step 2 -
$$\frac{6670*40[\Delta T]}{1000}$$
 = 267 lbs, the weight of steam

Step 4 – from steam consumption chart – The CTE2 $\frac{3}{4}$ unit will handle 6 lbs/min, the steam may be throttled back to reduce the rate of steam consumption to the desired 4.45 lb/min.

NOTE

Multiple units can be used if desired. Select smaller units with total steam consumption equal to or greater than the desired flow rate obtained in Step 3.



HEATING LIQUIDS IN LINE

MODELS CTE2

Method 2

The method can also be used in selecting the CTE2 heaters.

- Step 1 Divide the total batch gallons to be heated by the time (in minutes) required. This result is the gallons heated per minute.
- Step 2 Refer to the performance chart. In the column under required available operating steam pressure select the figure equal to or greater than the desired capacity. Check to determine if adequate temperature rise is possible with this size. If not, move down to a larger size.
- Step 3 If multiple units are desired, select several smaller heaters with a total capacity of that required.

Method 2 example

Though the following example illustrates the selection of a CTE2 heater

Operating conditions

Available steam pressure psig (h_m): 80 Desired temperature rise °F (Δ T): 40 Tank capacity, gallons: 10,000 Heating time, minutes: 35

Step 1 -
$$\frac{10,000}{35}$$
 = 286 gallons heater per minute (ghpm)

- Step 2 From performance chart under 80 psig steam pressure, go down the column to the capacity that is equal to or rater than required, to a row where T=40F. In this case the required capacity is 286 ghpm and the closest (higher) one is 315 ghpm in a 3" CTE2 heater.
- Step 3 If multiple units are required, try several smaller heaters, for example five 1 $\frac{1}{2}$ " units with 67 ghpm capacity: 5 x 67 = 355 ghpm total.



Table 16 - CTE2 PERFORMANCE (gallons heated per minute - ghpm)

	Temp. rise	Operating steam pressure (h _m)									
Size	°F (\(\Delta\T\)	20 psig	40 psig	60 psig	80 psig	100 psig	120 psig	140 psig			
	Ι (ΔΙ)				CTE						
	10	24	37	51	64	77	90	103			
	20	12	19	25	32	38	45	51			
3/8	40	6	9	13	16	19	22	26			
	80	3	5	6	8	10	11	13			
	120	2	3	4	5	6	8	9			
	10	51	78	106	133	160	187	214			
	20	25	39	53	67	80	94	107			
3/4	40	13	20	27	33	40	47	54			
	80	6	10	13	17	20	23	27			
	120	4	7	9	11	13	16	18			
	10	103	158	215	270	324	380	434			
	20	51	79	107	135	162	190	217			
1 1/2	40	26	40	54	67	81	95	108			
	80	13	20	27	34	41	48	54			
	120	9	13	18	23	27	32	36			
	10	203	214	425	534	642	752	859			
	20	102	157	212	267	321	376	429			
2	40	51	78	106	133	160	188	215			
	80	25	39	53	67	80	94	107			
	120	17	26	35	44	54	63	72			
•	10	481	741	1004	1261	1517	1777	2029			
	20	240	371	502	631	758	888	1015			
3	40	120	185	251	315	379	444	507			
	80	60	93	125	158	190	222	254			
	120	40	62	84	105	126	148	169			



HEATING LIQUIDS IN LINE

Table 17 - CTE2 STEAM CONSUMPTION (lbs per minute using dry steam)

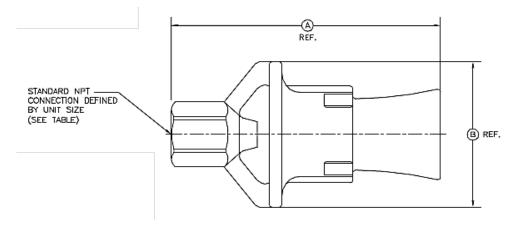
	Operating steam pressure (h _m)								
Size	10 psig	20 psig	40 psig	60 psig	80 psig	100 psig	120 psig	140 psig	
	CTE								
3/8	1	2	3	4	5	6	7	8	
3/4	2	4	6	9.5	11	13	16	18	
1 1/2	4	8	13	19	22	27	32	36	
2	6	17	26	36	44	63	63	71	
3	20	40	52	86	106	126	148	169	

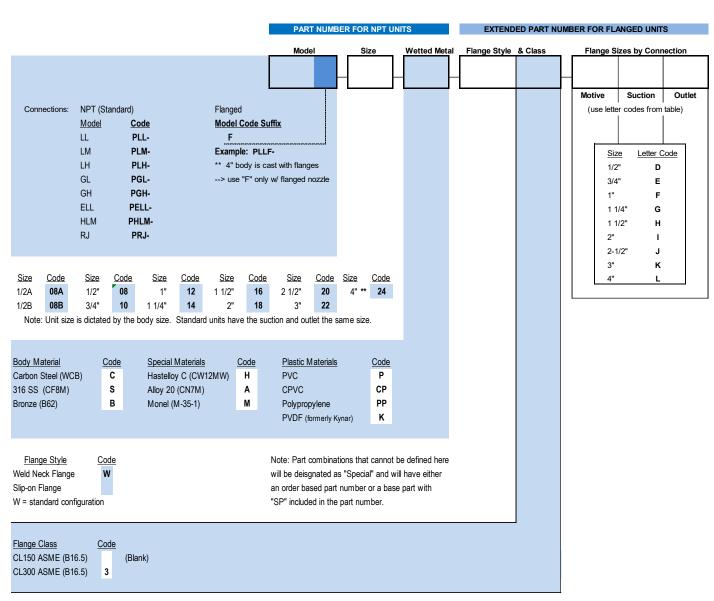


Table 17 - CTE2 DIMENSIONS (in inches)

Heater size	Α	С	D
3/8*	4 3/8	2 1/2	3/8
3/4*	7 3/8	3 3/4	3/4
1 1/2	11	5 1/2	1 1/2
2	14 5/8	7 3/4	2
3	22	11 3/4	3

*Male NPT

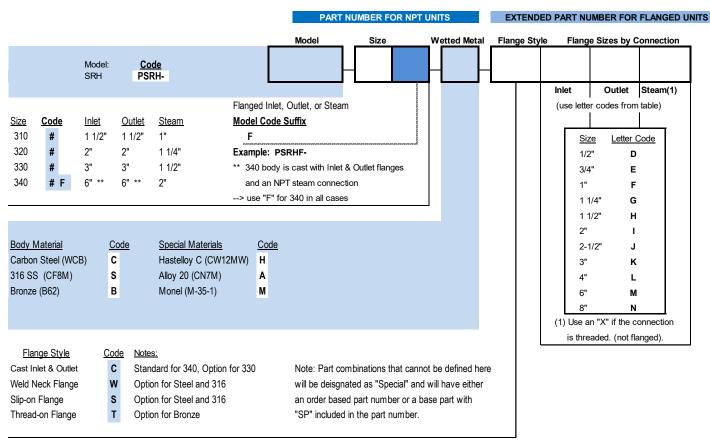




Examples:

- 1) 3/4" Model LM in bronze, standard connections
 - Part number: PLM-10-B
- 2) 1-1/2" Model LH in carbon steel with CL150 flanges, WN style, with standard 1-1/4" x 1-1/2" x 1-1/2" connection sizes Part number: PLHJ-16-C-W-GHH
- 2" Model GL in 316SS with CL300 flanges, WN style, with standard 1-1/2" x 2" x 2" connection sizes Part number: PGLF-18-S-W3-HII
- 4) 4" Model LM in carbon steel with standard NPT nozzle and CL150 flanged body (which is the only CL available for 4" body)
 Part number: PLM-24-C
- 5) 4" Model LM in carbon steel with flanged nozzle and CL150 flanged body (which is the only CL available for 4" body) Part number: PLMF-24-C-W-KLL





Examples:

1) Size 31 Model SRH in bronze, standard connections (1 1/2" x 1 1/2" x 1")

Part number: PSRH-31-B

2) Size 32 Model SRH in carbon steel, standard connections (2" x 2" x 1 1/4")

Part number: PSRH-32-C

3) Size 33 Model SRH in 316 SS, Standard connections (3" x 3" x 1 1/2")

Part number: PSRH-33-S

4) Size 33 Model SRH in Steel, Flanged inlet and outlet connections (3" x 3"), and a 1 1/2" flanged steam connection, all slip-on Part number: PSRH-33F-C-SKKI

5) Size 33 Model SRH in Bronze, Flanged inlet and outlet connections (3" x 3"), and a 1 1/ 2" NPT steam connection Part number: PSRH-33F-B-CKKX

5) Size 34 Model SRH in 316 SS, Standard connections (6" x 6" x 2")

Part number: PSRH-34F-S-CMMX

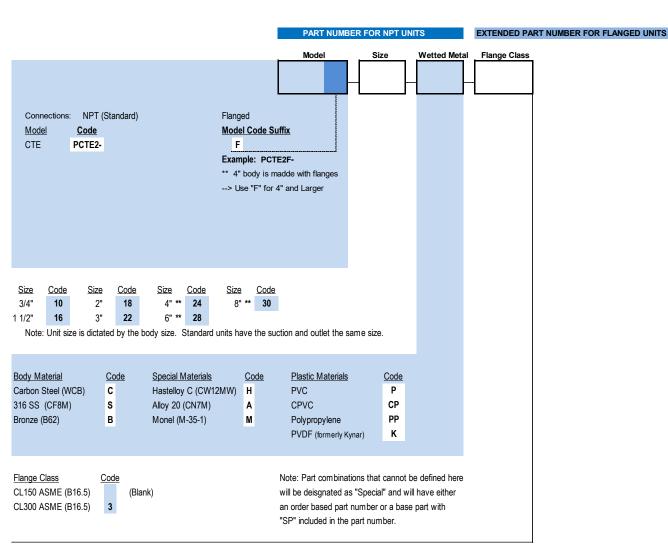
6) Size 34 Model SRH in Steel, Standard inlet and outlet connections (6" x 6"), and a 2" flanged steam connections, threaded

Part number: PSRH-34F-S-TMMX

Since the 340 has cast flanges, btu the steam can be standard NPT (X), then have a threaded (T) r slip-on (S),

We will use the variable connection in the part number.





Examples:

1) 3/4" Model CTE2 in bronze, standard connections

Part number: PCTE2-10-B

 1-1/2" Model CTE2 in carbon steel with CL150 flanges, 1-1/2" connection size Part number: PCTE2-16-C

3) 2" Model CTE2 in 316SS with CL300 flanges, with standard 2" connection size Part number: PCTE2-18-S-3

4) 3" Model CTE2 in 316 SS with CL150 flanged connection size

Part number: PCTE2F-22-S

5) 4" Model CTE2 in carbon steel CL150 flanged connection size

Part number: PCTE2F-24-C



